Choke Valve Decision Guide

Scope and action plan April 5, 2017



Mcilvaine Company Northfield, IL

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Choke Valve Decision Guide description and goals

 Mcilvaine is compiling a continually updated decision guide for operators of choke valves used in oil and gas and other industries for fluid control. Contaminants such as sand integrated into varying mixtures of water, oil, methane and other gases provide both operational and maintenance challenges. The guide identifies the major applications and then the performance of various designs and various materials for specific conditions... The wisdom of the industry is sought in order to make this guide the best it can be. Input is welcomed from any and all sources. For more information contact Bob Mcilvaine at rmcilvaine@mcilvainecompany.com 847 784 0012 ext 112



Spectrum of applications

Locations	fluids	equipment	service	Trim shape	Design flow	Conditions
surface	Oil	Well heads	production	Needle/disk	angle	Wet CO2
Sub sea	gas	Christmas tree	reinjection	cage	In-line (control)	Sour (High H2S)
chemical	Mixtures of crude oil, gas, water, sand	Manifold'		plug	Axial control but not choke service?	Abrasion, erosion, cavitation
petrochem	Steam, CO2			In line ball?		freezing
refineries	Drilling mud, Hydrauic Fracturing					

What are the applications? Why do some companies show axial control and axial choke as two different products when construction seems similar? What are the uses in chemical and petrochemical? Need info on produced water, fracking, drilling mud and all the applications



Choke valve Suppliers

Company	Descriptor axial	Descriptor angle	size	Max pressure psig
Cameron			1"-6"	10,000
Carter				
Circor	In line choke ball			
CCI (IMI		plug		
Flowserve				
FMC				
Master Flow	Diver or ROV retrievable		1"-10"	20,000
Mokveld				
N-Line	Distinguish between control and coke		2"-16"	20,000
Pentair				
Samson				
Subsea Chokes			4"-10"	20,000



Choke Definition

A **choke valve** is a particular design of <u>valve</u> that raises and lowers a solid cylinder (called a "plug" or "stem") which is placed around or inside another cylinder that has holes or slots. The design of a choke valve means fluids flowing through the cage are coming from all sides and that the streams of flow (through the holes or slots) collide with each other at the center of the cage cylinder, thereby dissipating the energy of the fluid through "<u>flow impingement</u>". The main advantage of choke valves is that they can be designed to be totally linear in their flow rate.

Choke valves are severe service valves which are designed specifically for oil and gas wellhead applications, both in a surface and subsurface context. They are used for controlling the flow on production, reinjection and subsurface wellheads. Choke valves are subjected to typical wellhead extreme conditions which can cause erosion, corrosion and other damage. Typically this can include high fluid velocity, slugging, sand production and multiphase of oil, gases and water. Also a choke valve has to have a very high turndown capability as it has to cover a wide range of flowrates. Thus the design of choke valves is required to be very robust with careful selection of valve configuration, flow path profiles, materials and ease of maintenance.

In subsea applications the choke valve has to cope with severe marine environmental conditions and be designed for subsea robot maintenance. If choke valves are selected poorly maintenance becomes a real issue with valves having to be removed regularly which is a real cost impost. Chokes can be operated manually or automatically. Sometimes a "choke bean" size is detailed, this is a device placed in a choke line that regulates the flow through the choke. Flow depends on the size of the opening in the bean; the larger the opening, the greater the flow.

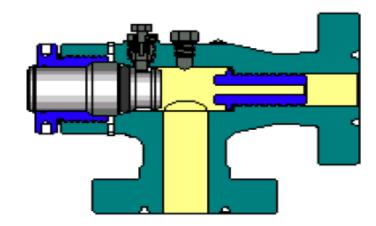
Actuator selection is also important, actuators may be a "stepping type" or linear depending on the valve design. Control systems can be complex on large facilities where multiple wells are controlled to production and reinjection manifolds.



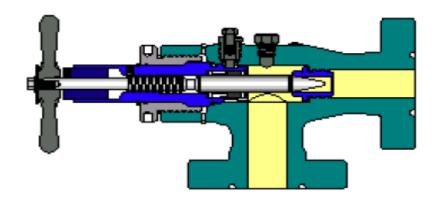
TYPES OF CHOKES?

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A positive choke has a fixed orifice size.
 Even though fixed chokes are available in a wide variety of sizes and types, the choke must be disassembled to change bean sizes.



 An adjustable choke provides variable orifice sizes through some type of external adjustment device.







Choke Design

Chokes hold a backpressure on a flowing well to make better use of the gas for natural gas lift and to control the bottom hole pressure for recovery reasons. In vertical pipe flow, the gas expands rapidly with decreasing hydrostatic head and the liquid moves in slugs through the tubing. The potential gas lift energy is rapidly lost and liquids fall back and begin to accumulate over the perforations. Accumulating liquids hold a back pressure on the formation. If enough liquids accumulate, the well may "die" and quit flowing.

A choke holds back pressure by restricting the flow opening at the well head. Back pressure restricts the uncontrolled expansion and rise of the gas and thus helps keep the gas dispersed in the liquids on the way up the tubing. Chokes may be variable or have a set opening. The set openings, often called "beans," are short flow tubes. They are graduated in 64ths of an inch. Common flow sizes are about 8 through more than 20 (in 64ths) for small to moderate rate gas wells. Liquid producers and high rate gas wells us 20+ choke settings. The size of the choke needed depends on reservoir pressure, tubing size, amount of gas, and amount and density of liquids. Variable chokes may use a increasing width slot design that allows quick resetting. They are useful on well cleanups following stimulation where choke size can vary over the course of a single day from 4/64ths to over 40. They are also used where periodic liquid unloading necessitates frequent choke size changes.



Choke function and problems

Solids in the produced fluids are the major source of failures for chokes. Abrasion from sand, scale, ice, corrosion particles and other solids can cut out the choke restriction and cause the well to load up with fluids and die.

Choke abrasion from solids and cavitation is increased when large pressure drops are taken. In these situations, choke life is often measured in minutes. For better performance at high pressure drops, take the drop in stages across three or more choke sets in series. The problem is with gas expansion; as gas goes from 5000 psi to atmospheric pressure, the gas expands 340 fold, with a similar increase in velocity. The same pressure drop, taken in series from 5000 to 3000, from 3000 to 500 and 800 to atmospheric results in gas volume (and velocity) increases of 136 fold (5000 psi to 3000 psi), 150 fold (3000 psi to 800 psi) and 54 fold (500 psi to atmospheric). The 340 fold total drop is the same, but the velocity increase across any one choke is significantly reduced.



Dealing with sand -Pentair

- Oil & Gas Choke valves or Control valves are extensively used in the petrochemical and process industries for the regulation of fluid flow. They experience a wide range of operating environments. Some of these operating conditions are extremely aggressive being not only corrosive but also erosive due to entrainment of sand in to the production flow. These are referred to as severe service conditions in oil & gas industries.
- Sand production is a known problem in the oil & gas industry. This produced sand carries through chokes (Control Valves) present
 in wellheads. Chokes are typically suffering for this in form of erosive damage. The erosive damage is decided by many different
 factors where the flow rate velocity of the fluid, sand rate, thermodynamic properties of the service conditions, fluid flow pattern,
 flow directions & materials are important ones.
- Dedicated effort is required to counter the control valve erosion to be able to maintain oil & gas production at an optimal level
 with attention to avoid unscheduled maintenance, safety and availability of other equipment also. Use of Computational Fluid
 Dynamics (CFD) has been essential in this work by simulating fluid flow through the control valves for optimizing the design,
 choosing the optimal erosion resistant material, coming up with improved erosion-related models and better mechanised
 operational procedures of the control valves.
- From the present simulation analysis of erosion wear the importance of pressure drop, flow velocity and flow pattern is analysed. Erosion rate is analysed for a 51mm bore (2, 1/16" 5000 psi) choke valve as up to 0.24 mm per year for a 50% valve opening.



Erosion Considerations - Pentair

The production part of oil & gas extraction platform involves topside & subsea manifolds arrangement. These manifolds is an assembly of equipment including tubing head adapters, valves, tees, crosses, top connectors and chokes attached to the uppermost connection of the tubing head used to control well production in oil & gas industries. They are rated for working pressures of 14 Mpa (2000 psi) to 103 Mpa (15,000 psi). Choke is the only device used to limit the production of flowing fluids. Chokes hold a back pressure on a flowing well to make better use of compressible fluid such as natural gas lift and control the bottomhole pressure for recovery reasons. In vertical pipe flow, gas expands rapidly with decreasing hydrostatic head and the fluid moves in slugs through the tubing. Solids in the produced fluids (Natural gas) are the major source of failures of chokes. Abrasion from sand, scale, ice, corrosion particles and other solids can cut through choke restriction and cause the well to load up with fluids and solids.

Pentair conclusions

Erosion in choke valves operating either in top side or subsea field subjected to sandy severe service conditions are considered as problems in oil & gas industries.

- 1. Critical location of the choke valve is trim components subjected to higher pressure drop also experiences higher flow velocity causes erosion in choke valves.
- 2. Particulate erosion in mainly due to jet impingement of sand particles inside the trim components of choke. Higher velocity causes the jet impingement.
- 3. Sand erosion rate is higher with increased pressure drop in low percentage valve openings.
- 4. Fluid flow pattern and sand particle sizes, hardness also influences in erosion rate for choke valves.



TRIM TYPES

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Needle and Seat

- o Simplest and least expensive adjustable choke
- Best for pressure control
- Reasonable capacity

Multiple Orifice Valve (MOV)

- Quick open and close (90 degrees)
- Good rate and pressure control
- Available as in-line installation

Fixed Bean

- Best for applications requiring infrequent adjustments
- Used mostly on wellhead Christmas trees

Plug and Cage

- High capacity
- Good controllability

External Sleeve

Reduced Capacity when compared to the Plug & Cage Design





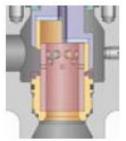


Multiple Orifice



Fixed Bean









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INFORMATION REQUIRED TO SIZE & SELECT A CHOKE

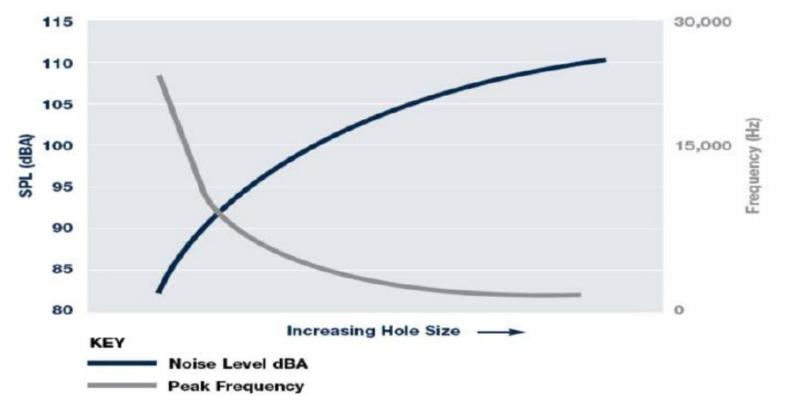
Application:	Produ	iction Chok	(e Valves	Process Fluid			
				Contaminates			1
				Maximum	Normal	Minimum	Start Up
	Limited	Oil	Units				
Flow rate	Liquid	Water					
	Gas / Va	pour					
	Inlet						
Pressure	Outlet						
	Delta p						
Temperature	Inlet						
	Specific Gravity						
Oil	Vapour Pressure						
	Critical Pressure						
	Viscosity						
	Specific						
Liquid	Vapour F	Pressure					
Liquiu	Critical Pressure						
	Viscosity						
		ar Weight					
Gas / Vapour		sibity (z)					
	Specific	Heat Ratio (γ)					





SMALL HOLE SIZES

- o Small holes increase peak frequency.
- Larger jets produce low frequency noise







INFORMATION REQUIRED TO SIZE & SELECT A CHOKE

Application:	Water Injection /	MEG Injection	Process Fluid			
	Choke Valves		Contaminates		_	
			Maximum	Normal	Minimum	Start Up
Flowrate	Liquid	Units				
	Inlet					
Pressure	Outlet					
	Delta p					
Temperature	Inlet					
	Specific Gravity					
Liauid	Vapour Pressure					
Liquid	Critical Pressure					
	Viscosity					





INFORMATION REQUIRED TO SIZE & SELECT A CHOKE

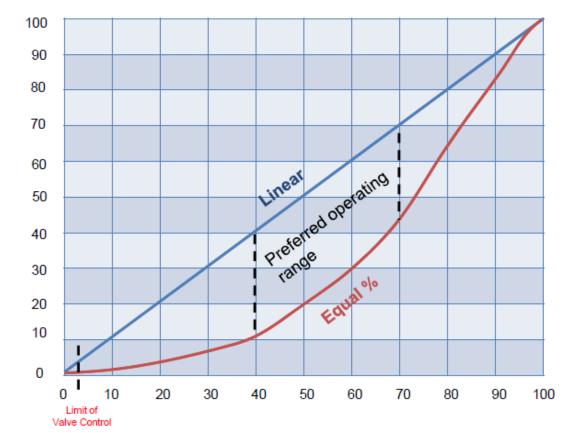
Application:	Gas Lift Ch	oke Valves	Process Fluid			
			Contaminates			
			Maximum	Normal	Minimum	Start Up
Flowrate	Gas / Vapour	Units				
	Inlet					
Pressure	Outlet					
	Delta p					
Temperature	Inlet					
	Molecular Weigh					
Gas / Vapour	Compressibility (z					
	Specific Heat Rat	io(γ)				
All Applications						
Line Size	<u>In</u>		Out		Schedule	
Valve Specificat	tion Details:					
End Connection	ns Size and Style					
Temperature Ra	atings (Min / Max)					
Choke Pressure	e Rating (psi)	3,000	5,000		10,000	1 5,0
Material Class F	Ratings	□ 'cc'	☐ 'EE'		'FF'	□ 'HH'
PSL Level		PSL 2	☐ PSL3	3 🗖	PSL 3G	☐ PS
Mandatory Req	ulrements		Pressure 8	k Temperature U	Inits to be specif	led by the customer
		e start up conditions			, , , , , , , , , , , , , , , , , , , ,	,
Full information a	allows detailed applie	ation review and correct tri	m / choke selection		_	
r uii illioithadon a	anows detaned applic	auon review and correct un	III7 CHOKE SEIECTION			



TRIM CHARACTERISTICS – LINEAR & EQ%

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Valve Lift % of Full Lift

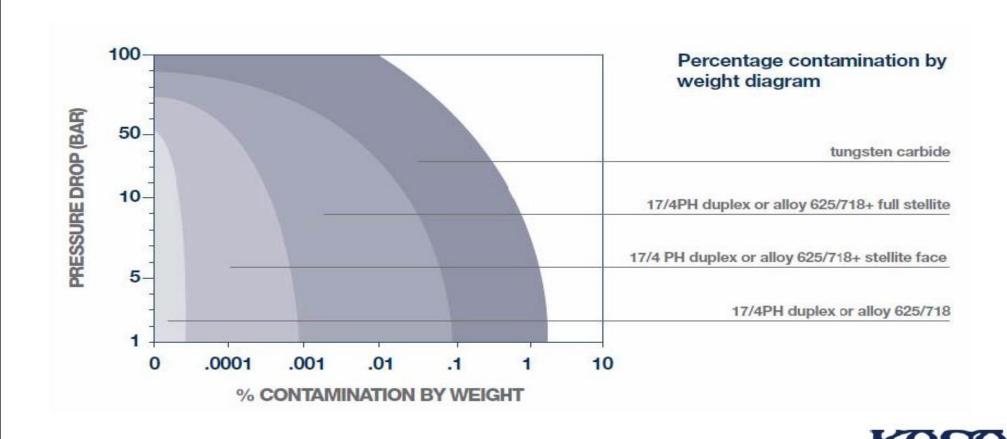




VELOCITY CONSIDERATIONS

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Trim Material Selection Due to Contamination





VELOCITY CONSIDERATIONS

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Table 3. Recommended Maximum Velocities for **Liquid** Service

Choke Size		Maximum Recommended Velocity				
		Low Al	loy Steel	High Alloy Steel		
Ins.	mm	ft/s	m/s	ft/s	m/s	
2 - 8	50 - 200	48 (65)	14.6 (19.8)	6 (19.8) 57 (75) 17.4 (2		

Note: Values in brackets refer to Centre Module Limits.

Table 4. Recommended Maximum Velocities for Gas/Vapour Service

Choke Size M		Maximu	ım Inlet	Maximu	m Outlet	Maximum	Outlet Mac	h Number for
	Velocity		Velocity Velocity		Red	uired Noise	Level	
Ins.	mm	ft/s	m/s	ft/s	m/s	>95 dBA	<95 dBA	<85 dBA
2 - 8	50 - 200	475 (670)	144 (204)	830 (1150)	253 (350)	0.65 (0.9)	0.5 (0.7)	0.3 (0.5)

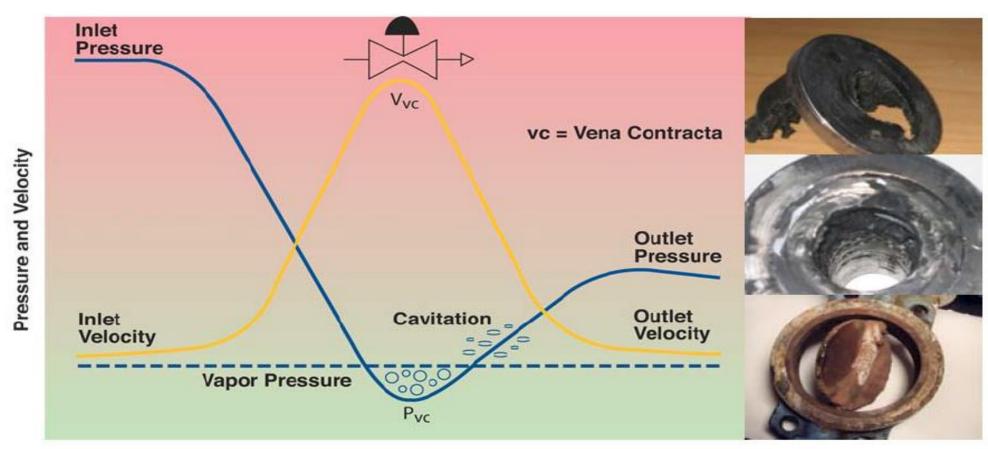
Note: Values in brackets refer to Centre Module Limits.

- General Recommendation for Choke Valves with Clean Fluids.
- Note: For In-Line Chokes these figures should be reduced, especially if solid contaminates are present.



CAVITATION – SINGLE STAGE TRIM

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Profile Through Valve

https://www.youtube.com/watch?v=2k1NRCRVZZM

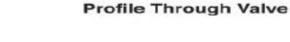


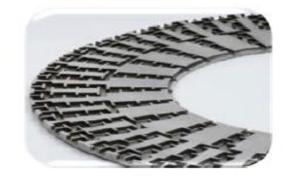
VELOCITY CONTROL ELIMINATES kentintrol PROBLEMS:

Vibration, erosion,
noise threshold

Vibration, erosion,
Vibration, erosion, erosion,
Vibration, erosion, e





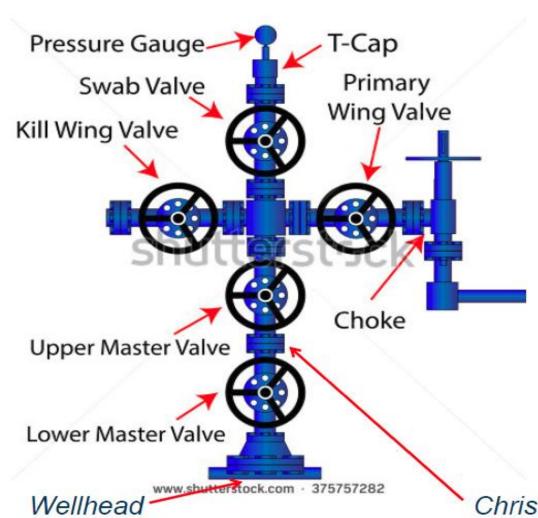






GETTING THE OIL & GAS OUT

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Christmas Tree or Wellhead?

A Christmas Tree is an assembly of valves, spools, and fittings used for an oil well, gas well, water injection well, water disposal well, gas injection well, condensate well, and other types of wells. It is named for its resemblance to a decorate tree at Christmas.

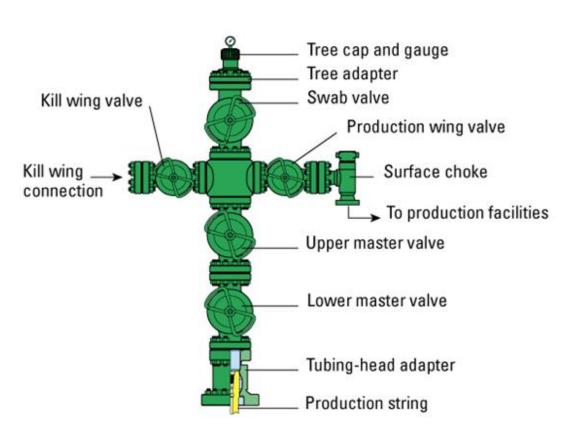
Many times, the words Christmas
Tree and Wellhead are used
interchangeably; however, a wellhead
and Christmas tree are entirely
separate pieces of equipment. A
wellhead must be present in order to
utilize a Christmas tree and is used
without a Christmas tree during
drilling operations.

Christmas Tree





Choke Valve in Christmas Tree



- In this Christmas Tree Diagram there are five valves. The Kill Wing valve, the Swab valve, the production wing valve, the upper master valve and lower master valve. When the operator, well, and facilities are ready to produce and receive oil or gas, valves are opened and the release of the formation fluids is allowed to flow into and through a pipeline.
- The two lower valves are called the master valves (upper and lower respectively) because they lie in the flow path, which well fluids must take to get to surface.
- The lower master valve will normally be manually operated, while the upper master valve is often hydraulically actuated.
- Hydraulic tree wing valves are usually built to be fail safe closed, meaning they require active hydraulic pressure to stay open.
- The right hand valve is often called the flow wing valve or the production wing valve, because it is in the flow path the hydrocarbons take to production facilities.
- The left hand valve is often called the kill wing valve. It is primarily used for injection of fluids such as corrosion inhibitors or methanol to prevent hydrate formation.
- The valve at the top is called the swab valve and lies in the path used for well interventions like wireline and coiled tubing.
- A 'Choke' is a device, either stationary or adjustable, used to control the gas flow, also known as volume, or create downstream pressure, also known as back pressure



Cameron Multiple Orifice choke valves

Cameron Multiple Orifice Choke Valves

- Cameron's Multiple Orifice Valves (MOVs) together with four special trim designs incorporate materials to meet the tough conditions including cavitation, erosion, and freezing, three of the greatest threats to efficient flow control operations.
- Cameron has an extensive database and can select the proper materials and alloys for specific choke applications.
 Continuing investigations to determine the relative erosion, abrasion, and cavitation resistance characteristic of materials allows Cameron to develop improved choke technologies for enhanced durability and wear resistance.
- The effects of abrasion, erosion, and cavitation can be reduced by applying hard facing to the interior surfaces of the choke outlet or by using an extended wear sleeve in the outlet.
- Specific grades of tungsten carbide are effective at reducing erosion wear, while StelliteTM is most resistant to the destructive consequences of cavitation.



Cameron MOV special designs for each application

The purpose of the MOV is to provide accurate, calibrated flow control and increased choke service life in all applications, including erosive conditions. Toward that goal, new disc designs have been required to meet new and greater demands of better rangeability, higher capacity, and increasingly severe conditions. These new disc designs involve altering the normally round orifice shapes on the discs to adapt them for special conditions. With practically every drilling job, large cuttings come up the casing with the mud. The cuttings can block the throttling restriction in many chokes. However, Cameron's drilling choke trim is specially designed for mud service. Utilizing a half-moon shaped hole, the drilling choke trim rotates through a control range from fully open to fully closed in 180 degrees. This design delivers control so reliable that the drilling choke outperforms other designs for well killing and pressure control, especially in severe service involving H2 S, abrasive fluids, and high pressures.

- 1. Style 0 Standard Service Standard service valves are the lowest cost choke styles. They generally are intended for sweet crude oil, deaerated water, sweet natural gas, and other non-corrosive fluids.
- 2. Style 8 Sour Service In addition to the requirements of the standard valve type, the materials of the pressure containing parts of this style meet the requirements of NACE MR-01-75. Sour service chokes are intended for applications with H2 S present as defined by NACE MR-01-75 requirements
- 3. Style 4 Wet CO2 Service This type of choke is intended for applications and service with wet CO2 (sweet or sour) and other applications where 410 or 316 SS is accepted. All wetted pressure-containing parts are made of stainless steel.
- 4. Style C Low Temperature/Sour Service In addition to the requirements of standard and sour gas service chokes, the requirements of API 6A specifications are met. This adds Charpy impact testing of materials for pressure containing parts. These valves are intended for cold -50° F (-46° C) flow and/or ambient conditions, with or without sour service.



Cameron MOV applications

- Cameron's extensive MOV line covers 1" to 6" (25 mm to 152 mm) sizes that can handle pressures up to 10,000 psi while operating at temperatures ranging from -50° F to 650° F (-46° C to 343° C). They are manufactured to meet API, ANSI, and NACE standards. MOVs are available in both adjustable and positive configurations with a variety of end connections to meet most requirements, as well as angled and in-line body configurations.
- The near-linear flow characteristics of the MOV make it well suited for production choke applications including:
- Wellhead Attached to the wing valve on the Christmas tree, and provides great control for oil and gas production.
- Manifold Used to maintain pressures and control flow rates in oil or gas production systems, and for pressure control in choke and kill manifolds.
- Separator Letdown Used as a quick open/quick close quarter-turn valve to maintain levels in separators.
- Heater Bypass Used on a secondary bypass loop to reduce and control gas pressure.
- Water Flood Used to control injection rates for pressure maintenance and enhanced oil recovery (EOR). CO2 Provides accurate injection control for EOR with great resistance to freeze up.
- Gas Lift Used to maintain pressures and control gas injection rates in a well to aid in oil production.



Carter Process Control GmbH (CPC), Austria, offers trim

- Carter Process Control GmbH has designed and engineered (Patent Pending) a Solid Tungsten Carbide multi Stage Severe Service Trim for Control Choke Valves with "NO" brazing, EDM or Erosion.
- JACK Trim—Solid Tungsten Carbide 6% cobalt (1-3 micron WC) Plug—Solid
 Tungsten Carbide 6% cobalt (1-3 micron WC) Seat Ring—Solid Tungsten Carbide
 6% cobalt (1-3 micron WC) or insert Stem—Duplex (F51), Inconel or other as
 required
- As a non valve manufacturer but with extensive control valve trim manufacturing experience CPC is uniquely positioned to supply its trim to any valve manufacturer or end user that requires a severe service multistage pressure reduction trim. Available in an almost limitless range of sizes and pressure reduction stages to fit the most arduous of operating conditions.

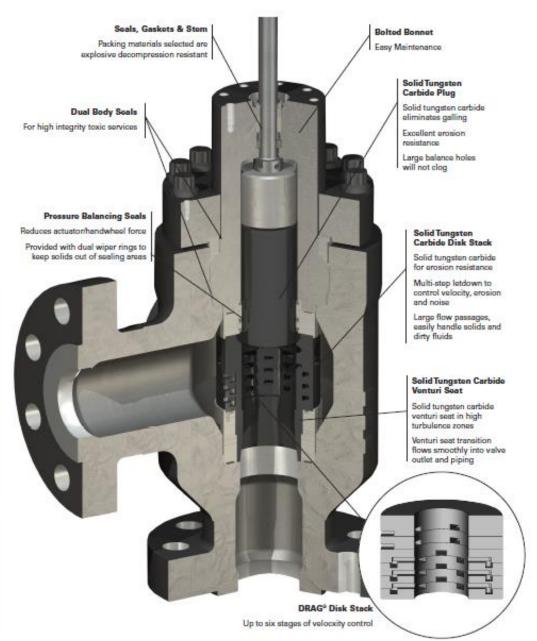


CCI Profile

• CCI DRAG® Technology for Severe Service Choke Valves - Today's gas field environment means higher wellhead pressures with aggressive fluids with entrained sand and other solid particles. A conventional single stage choke valve is not suitable for this kind of severe service. The need to maintain production rates means that frequent choke repair or replacement is no longer acceptable. CCI has the world's first true severe service choke valve that uses a combination of proven DRAG® velocity control technology and the best grades of tungsten carbide material used in the industry to provide long trim life and precise process control.



CCI Choke features





Problems solved with CCI drag choke

Requirement	Conventional Choke Valve	Root Cause(s)
Operation at high pressure differentials for extended periods of time.	Production time significantly reduced due to frequent repair or replacement of trims and/or bodies.	Inadequate control of fluid velocities resulting in rapid damage to trim components.
Improved control at wellhead.	Inability to precisely control pressure and/ or flow.	Poor rangeability inherent to design. Inadequate control of fluid velocities resulting in high erosion rates and rapid damage to control surfaces of trim components.
Improved resistance to erosion due to sand and other particulate matter entrained in fluids.	Production time significantly reduced due to frequent repair or replacement of trims and/or bodies.	Inadequate control of fluid velocities resulting in high erosion rates and rapid damage to trim components. Poor material selection.
Ability to accommodate significant changes in well operating conditions over time.	Replace existing valve to address new well operating conditions.	Poor rangeability. Inability to significantly modify existing valve.
Safety and reliability for increasingly demanding and challenging environments.	Operation of facility and health of employees compromised due to rapid erosion to pressure boundary parts, severe mechanical vibration and excessive noise.	Inadequate control of fluid velocities.



Design comparison

See the following CCI chart and provide feedback relative to

- Tungsten carbide for plug, disk stack etc
- Passage size
- Multi step let down
- Stroke length
- Number of scrapers
- Transition shape
- Interchangeable trim
- Number of stages



Benefits of CCI choke valve vs competitors

	Benefits	CCI 100DPC DRAG® Choke Valve	Competitors
1	Solid tungsten carbide plug, seat and disk stack eliminates erosion and galling and extends performance life for maximum productivity.	✓	
2	Large flow passages to easily handle solids means continued reliable performance.	✓	
3	Multi-step letdown to control velocity, erosion, noise, and vibration for minimum down time and safety.	✓	
4	Increased rangeability due to a longer stroke means superior performance and control.	\	
5	Dual scrapers prevent solids from entering sealing areas for reduced maintenance.	✓	
6	Venturi seat transition assures smooth flow into valve outlet and piping for problems downstream.	✓	
7	Easy maintenance, quick-change trim means no trim parts are welded or screwed into the body.	✓	
8	One choke body can handle changing wellhead conditions by swapping trim for less down time.	✓	
9	Up to 6 stages of DRAG® velocity control (with total velocity control trim disk stack.)	✓	
10	All trim seals are PTFE. PTFE is explosive decompression resistant.	✓	



Choke valve short life can be extended with CCI

Wellhead choke valves, usually in sizes of up to 6in and in the API pressure range 5000 to 15,000, have long been considered an almost expendable item of equipment. Typically the life of choke valves can be very short. A matter of hours is not unheard of, although months is more common, but this is still unsatisfactory. The reason is complex, and only recently has it become comprehensively understood. Essentially, it is a system problem — the interaction of many factors which constantly change and produce a number of levels of overall instability and rapid wear out.

One of these factors is the composition of the fluid handled, which can change frequently and unpredictably. Another reason is design operating conditions that are appropriate today can change over time and may in a few years extend beyond the capabilities of the original valve design. These controlling factors largely exclude operating pressure and differential pressure as problem areas in choke valve design. Today, even at the high end of choke valve operating pressures, the industry has a vast store of high pressure applications experience that is equally applicable to choke valve service.

<u>Fluid composition</u>: The fluid handled is a mixture of crude oil, gas, water, sand, and often other solid components. Since the proportion of each component in the fluid mixture can change constantly, it is difficult if not impossible to accurately determine the actual effective fluid velocity because each of the components travels at a different velocity in the build stream. Therefore, velocity in the pure sense cannot be a useful as reliable choke valve design criterion. However, it is obvious that the sand, and perhaps other solids, is the bottom-line culprit in short choke valve life. But this is far from the whole story.

Changing operating conditions: While in time, choke valve flows are relatively constant, well head pressures change as the wells age. Usually, high operating pressures are associated with relatively stable down-well geological formations where less sand in released But as wellhead pressures start to fall, and these geological formations start to collapse, the percentage of the sand in the fluid flow can increase. In some cases, this decreasing pressure/ increased sand relationship can be inverted, further complicating the choke valve design process. In addition, decreasing operating pressures with relatively constant flow can increase the required valve coefficient Cv) by as much as a factor of 10, usually well beyond the original value's design capability. While common single-stage choke valves have attempted to achieve acceptable performance life through improved material, this has not been enough. As more and more large older wells are changing from oil to gas production, choke valve internal velocities ae increasing, exacerbating the erosive damage effect of the entrained sand. And as valve trim erodes as a result, control is compromised and the flow needed requires closer plug/seat operation. This, in turn, accelerates plug/seat erosion, regardless of materials. Another contributing factor is increased vibration (and related high noise levels) which the eroded valve trim and other operating circumstances can create. So, it is this vicious circle that plagues operations with extremely high maintenance costs and grossly unacceptable short choke valve life.



CCI Multi stage valve design advantages

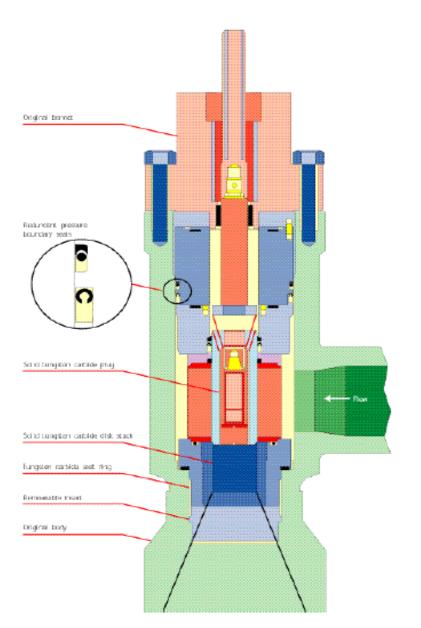
To limit fluid velocity throughout the valve trim and to drastically reduce the erosive effects of the sand, a multistage valve design uses a stack of disks, each of which incorporates a tortuous path flow pattern by means of a series of right-angle turns in each disk. The velocity of all fluid components is thereby cut by at least 75 per cent compared to single-stage plug / seat and drilled hole-cage designs.

By using tungsten carbine trim throughout, the erosive effects of the sand are minimized. In addition, long valve stem stroke increases range ability and enhances controllability, so that flow set points can be maintained and changes in operating conditions can be accommodated over time. These valves are also characterized, which means that the tortuous paths in discrete groups on individual disks in the disk stack are differently designed; that is, flow per disk in one group is higher or lower that in a disk in another group. The benefit in choke valve characterization lies in the ability to maintain a larger distance between the plug and the seat at low flows; pressure reduction is there for the same as that achieved within the tortuous path, multistage disks rather than by a throttling process through a small plug/disk annular clearance.

The use of this multistage valve technology and modern materials of construction have borne fruit. Valve life has been demonstrated to be up to 10 times greater than was expected previously, especially where sand content was high. This gain in choke valve life has been shown to be true for new, replacement and old valves that have been retrofitted with multistage characterized, longstroke all tungsten-carbine trim.



CCI Multi stage retrofitted with silcon carbide trim





CIRCOR PIBIVIESSE In-line Choke Ball

Hyper Cage	Hyper Cage Multistage	Hyper Silent	Cage Ball Orifile Plate	Inline Choke Ball
Pigable version Full and Reduced Bore	High Performance Full and Reduced Bore	High Noise Control Full and Reduced Bore	High Performance Full and Reduced Bore	Choke Conditions High Performance Full and Reduced Bore
6÷60" DN 150÷1500	6÷60" DN 150÷1500	6÷60" DN 150÷1500	6÷60" DN 150÷1500	1÷8" DN 25÷200
ASME Class 150÷2500# API 10000÷20000	ASME Class 150÷2500# API 10000÷20000	ASME Class 150÷2500# API 10000÷20000	ASME Class 150÷2500# API 10000÷20000	ASME Class 150÷2500# API 10000÷20000
• Flanged • Welded	• Flanged • Welded	• Flanged • Welded	• Flanged • Welded	• Flanged • Welded
Carbon Steel Low Temperature Carbon Steel Duplex Stainless Steel Incoloy 825 Inconel 625	Carbon Steel Low Temperature Carbon Steel Duplex Stainless Steel Incoloy 825 Inconel 625	Carbon Steel Low Temperature Carbon Steel Duplex Stainless Steel Incoloy 825 Inconel 625	Carbon Steel Low Temperature Carbon Steel Duplex Stainless Steel Incoloy 825 Inconel 625	Carbon Steel Low Temperature Carbon Steel Duplex Stainless Steel Incoloy 825 Inconel 625
Stainless Steel Inconel Duplex Super Duplex	Stainless Steel Inconel Duplex Super Duplex	Stainless Steel Inconel Duplex Super Duplex	Stainless Steel Inconel Duplex Super Duplex	Stainless Steel Inconel Duplex Super Duplex
 High range of process conditions Negligible ∆P at full stroke Tight shut-off requirements 	Low noise Cavitation control Velocity and vibration control High capacity and rangeability Tight shut-off requirements	High capacity of noise control Flow and pressure control Tight shut-off requirements	Pressure equalization High △P Flow and pressure control Tight shut-off requirements	Choke applications Tight shut-off requirements



Integrated gas lift system from Flowserve

- INTEGRATED CONTROL VALVE SYSTEMS BOOST ROI With "easy oil" diminished and the price of oil trending upward, it makes good engineering and business sense to optimize the gas-lift process by installing an integrated flow control gas injection system over manual choke or conventional automated control valve systems.
- This is because an integrated solution decreases the consumption of gas and energy while increasing the recovery rates of the oil and gas. Under the right circumstances, a return on investment can be realized in a matter of days, paving the way for a boost in revenue and reduction of costs.
- We want to pursue details on the integrated system from Flowserve and the input from others on trhe importance of the solutions approach



FMC Technologies actuator and throttle valve

Electric Choke Actuator

- In the years since FMC began development of electric solutions, options for several subsea applications have been released. The first application, installed in 2001 and 2002, was an electric choke actuator for Statoil's Statford Satellite project.
- This consists of electric choke controls and a sand detection system connected to a central electric control module. The field originally featured only ROV-operated chokes, and production adjustment of individual wells could not be done as frequently as the operator wanted. Installing electrical actuators and sand detectors proved efficient. The system was installed without production shutdown and works with the existing electro-hydraulic controls. It has had nearly 100% up-time to date. Electric choke actuation is efficient and simple. Traditional electro-hydraulic choke controls may use stepping actuators. Each stepping actuator requires two hydraulic control valves in the electro-hydraulic control module, and some 200 steps (hydraulic pulses) to travel from fully closed to fully open.
- In StatoilHydro's Norne Retrofit project in the North Sea, FMC's actuator system operates manifold and pigging valves as well as the chokes. The electric manifold valves were a cost-efficient retrofit for Norne. The electrical equipment that replaced manually and hydraulically operated valves and chokes gives better response time for the chokes and enables free routing of existing and new infield wells. It also liberated hydraulic lines in an existing umbilical for use as injection chemical lines. Capital expenditures for the field extension were reduced significantly. Electric manifold valve control is attractive in systems where control modules can be eliminated from the manifold to completely eliminate the hydraulic distribution for the manifold which improves delivery time, simplifies testing, and reduces cost.

Weco Valves Choke Throttle Valves

• In high-pressure pumping applications throttling is often required to control hydraulic fracturing fluids. The choke throttle valve combines the best attributes of a ported cage choke and a plug valve. Pressure pumpers are now capable of throttling high velocity erosive fluids without degrading the positive shutoff performance of the valve. The Weco choke throttle valve is available in 1 inch at 15,000 psi CWP.

What about Electric actuators vs alternatives
Does the throttle valve combine the best attributes of a ported cage choke and a plug valve



SURFACE CHOKE VALVES

kentintrol



- o Sizes 2" 16"
- o ANSI CL 900 4500
- o API 3000 15000
- Carbide Trim Options
- Actuator Options
- Materials WCB, LCC, AISI
 4130, AISI 8630, F22, Alloy
 625, Duplex's
- o API 6A PR2 & API 17D Testing





CHOKE VALVE BODY ASSEMBLY kentintrol Stem Seal-Bonnet Body / Bonnet Seal Stem Body Lower Guide 'Brick Stopper' Resilient Seal Carbide Plug Head Carbide Guide **Body Trim Seal**



Master Flo Valve, Inc. Profile

- Products are engineered for surface and subsea environments and are installed on some of the most demanding production sites around the world.
 Range of applications, including high erosion, high pressure, high temperature, SAGD
- Choke valves range in price from \$1,000 to \$400,000. The costliest are large subsea units that have been used at water depths of up to 3,000 metres. Many of those are designed so they can be retrieved for service with remoteoperated tools.

Master Flo Choke valve applications

- Blow Down Separator blow downs / Level controllers, separator discharges
- Vent Valves Vent valves to flare
- Level Controllers High pressure drop level controllers, (or high abrasive applications
- Gas Lift and Injection Chokes used to control injection volumes
- Water Injection Injection Chokes with multistage trims available for large pressure drops
- Water Injection Recycle Lines High pressure drop liquid recycle lines with Master Flo's multistage trim
- Overboard Dumps High pressure drops with multistage trim
- Dump Valves Glycol Knock out drums / Separator dump valves
- Production Wellhead and Manifold choke
- Glycol Injection
- Well Cleanup

what is the range of pricing and what affects the price?

we need details on the applications mentioned such as overboard dumps, well cleanup. Vent valve to flare?



Master Flo Sub Sea Choke Valves

Equipment operates at depths of over 10,000 feet below sea level as well as high pressure, high temperature conditions, while maintaining high controllability and reliability.

Products range from:

- bolted bonnet
- diver insert retrievable
- ROV insert retrievable
- manual actuated
- stepping actuated
- linear actuated
- electric actuated
- all available in 1"-10" configurations with a wide range of feedback and monitoring options

Additionally:

- Single or multi-phase production
- Water/chemical/gas injection
- Artificial gas lift
- Anti-surge
- Closed loop flow control
- All choke and control valves can be provided as non-retrievable, diver retrievable or insert retrievable designs.
- This product range is also complemented by a full suite of onshore and offshore handling, test and intervention equipment which can be packaged to meet project requirements and be provided on a rental or purchase basis.



Master Flo Bolted-Bonnet Choke



- This choke valve is ideal for modularretrieval systems or applications where valve maintenance is not required. Rightangle, inline, or custom piping configurations are available to meet a variety of needs. This product is available in a wide range of sizes and pressures up to 20,000 PSIG.
- This choke may be set up for operation by diver or remotely operated vehicle (ROV). Alternatively, remote actuation is also available). An additional option is an electrical position transmitter.



Master Flo Diver Choke Valve



 This choke is intended for water depths that are suitable for diver intervention. It features a diver-operated dual-stem clamp connector that secures the choke internals to the valve body. This allows the choke insert to be retrieved to surface for maintenance. Doubletapered metal seals are used for reliable sealing of the bonnet to the body. This product is available in a range of sizes and pressures up to 10000 PSIG. This choke may be set up for operation by diver or remotely operated vehicle (ROV). Alternately, remote actuation is also available (please see our actuation page for more details). An additional option is an electrical position transmitter.



Master Flo Insert-Retrievable Chokes

- HRV chokes are qualified for water depths up to 11,000 feet (3,350 m) and are available for pressures up to 20,000 psig (138,000 kPa). It consists of a right-angle body with an insert module that can be installed or retrieved by a cable-deployed running tool with the assistance of a remotely operated vehicle (ROV). The choke insert module (CIM) includes all of the valve internals, the actuator, and an ROV-operated clamp connector, which secures the insert to the valve body. Metal-to-metal seals are used at all critical sealing areas including a double-tapered metal bonnet seal. This product is available in a number of sizes and pressure/temperature ranges.
- The insert clamp connector (ICC) is available with either horizontal or vertical ROV access in several positions relative to the valve piping. This clamp system is designed so that, should it fail, the connector stem can be cut by an ROV-mounted tool thereby allowing emergency release of the insert module. Because this clamp connector is part of the insert module, it can then be repaired once retrieved to the surface.



Master Flow Surface Choke

Production

- with CO2
- with H2S
- with CO2 and H2S

Water Injection

- clean water
- brackish water
- seawater
- produced water

Gas Injection

- CO2
- Methane

Heavy Oil

- Production
- Steam injection
- SAGD

Top Side Process

 Choke at top of riser is usually used for flow split control to test and production or to throttle in to get pressure up and prevent slugging



Master Flo Valve Design Comments on agreement with these specs?

Design methodology, qualification and performance verification for production chokes is covered by the API specification 6A (ISO 10423) for surface equipment and API 17D for subsea equipment. These valves may be supplied with API, ASME or other (manufacturer specific) end connections. Valve ratings must specify pressure, temperature, material classification and capacity. These valves are typically pressure or flow restriction valves, therefore manufactured with reduced bores resulting in higher fluid velocity within the body bore. The higher velocity can have a dramatic effect on erosion and corrosion rates. Typically, the higher velocity within the valve requires special consideration be given to material selection since corrosion inhibitors may not be effective. Choke valves typically experience high velocity at the throttling mechanism; accordingly, the materials selected for the trim components must consider the service conditions. Applicable specifications will include API 6A, API 17D, ANSI B16.34, ANSI B16.5, ISA S75.01, ISA S75.02, ANSI/FCI 70-2, ASME IX and NACE MR 01 75 (ISO 15156).

- Valve design methodology shall conform to API 6A latest edition.
- Valve performance verification shall conform to API 6A PR2 and/or API 17D as applicable.
- Valve internals including trim components shall be held in position by the bonnet bolting. Valve designs that utilize threads to secure the seat to the body are not recommended.
- Valve design shall incorporate means for galling prevention on all dynamic sealing components. Metal to metal contact between sliding or rotating sealing components shall be avoided. In the case of metal seals the stem surface shall be protected with a suitable Tungsten Carbide coating to prevent galling.
- Capacity "Cv" rating shall be tested per ISA S75.02. Test results shall be accurate to within 5% of published data.
- Valve designs shall incorporate a sliding stem design. Designs that rotate stems within seals shall be avoided.
- Long valve travel is preferred for applications which require good controllability. For actuated applications long valve travel is required.
 Valve designs shall consider serviceability. Valves should be field serviceable without special tools.
- Valve designs shall consider serviceability. Valves should be field serviceable without special tools.



Master Flo Body Design Comments on agreement with these specs?

Choke bodies can be either a right angle design or an inline orientation; inline typically referred to as control valves. The angle type orientation is preferred for severe service applications. This orientation will allow improved fluid management since the fluid exiting the trim will travel directly into the valve outlet. The valve model is typically associated with the valve trim size as assigned by the valve manufacturer and therefore should not be the governing factor in valve selection. Proper valve selection should be based on valve capacity "Cv" as tested per ISA S75.02 verses flow condition requirements as calculated by ISA S75.01 methodology. Valve models may be smaller than the end connections supplied. Example: a 4" valve may be fitted with 6" end connections.

Body outlet profile shall be free of steps or abrupt change in diameters. Outlet sleeves, if necessary, must be accommodated with smooth transitions.

Screw-in seat assemblies shall not be used. Wetted threads should be avoided where possible.

Welded end connections are acceptable provided material selection and weld design conform to sound Engineering practice. All weld procedures must be ASME IX qualified. All alloy steel welds shall be stress relieved after welding.

Design may utilize a Hammer Union Nut Bonnet or Bolted Bonnet connection provided the Bonnet connection does not require special tools for valve disassembly.

Valves supplied with rotary actuators must utilize bolted bonnet designs.

In erosive applications a right angle body design is the preferred configuration.

End connections bores shall match mating flange bores/schedule to prevent unnecessary protrusions within the transition.

Valve model/size selected shall consider the effect of velocity on erosion and corrosion control.



Master Flo Trim Designs Comments on agreement with these specs?

Trim designs may be classified as needle and seat, disk, or cage designs. Important factors to consider in trim selection are controllability defined as the "turn down ratio"; pressure recovery factor defined as the "FL factor"; valve capacity defined as the "Cv."

Design shall incorporate cage type trim. Trim design can be cage with external sleeve or internal plug design. Erosive or high pressure applications shall utilize an external throttling sleeve. Internal plug designs are not recommended for erosive or high pressure drop applications.

Valve trim should be designed with equal percentage opening characteristics for improved controllability. Quick opening characteristics shall not be supplied for modulating service.

For erosive service the ports should be positioned on the valve axis to reduce turbulence around the cage. For non-erosive service multi-ported cages are acceptable.

The shut-off mechanism is to be segregated and upstream of throttling ports. The seating face shall be metal to metal.

Materials used for erosion protection shall be solid tungsten carbide for erosive conditions and hardened stainless steel for non-erosion applications. Stainless steel carriers are acceptable for the flow sleeve; however the entire turbulent area and high velocity zone shall be protected with hardened trim material. The Cage shall be of solid hardened trim material. Hard facing or overlay shall not be used.

Tungsten Carbide trim materials shall utilize composite binders considering both erosion and corrosion properties. Minimum hardness for the tungsten carbide shall be Ra 93. Binder constitutes shall be Nickel, Chromium and Cobalt at a minimum.

Multi-Stage trim designs shall utilize a throttling mechanism on each stage. Designs which throttle on the initial or final stage only are not acceptable.

Trim design shall consider the potential for plugging and the design shall incorporate suitable means for passing normal sand and proppant that may be present within the fluid media



Designs should consider life cycle costs. Designs which incorporate the trim components into the valve stem should be avoided.

Trim design shall be capable of Class V shutoff as defined by ANSI/FCI 70-2

Master Flo Actuators Comments on agreement with these specs?

Valve actuation may incorporate a manual operator (hand wheel) or pneumatic, hydraulic or electric actuators. For remote modulating operation the actuator is typically fitted with a positioner that will accept an input signal (either 3-15 psi, 6-30 psi or 4-20mA) to position the valve respective to the input signal. Linear actuators can incorporate fail positions defined as "fail open", "fail closed" or "fail last". This action is typically achieved through a mechanical spring, however in the case of linear hydraulic actuators; this can be accomplished through incorporation of an accumulator.

Typical positional accuracy for linear actuated valves shall be 2% of valve travel for pneumatic applications and 1% for hydraulic applications.

Typical positional accuracy for rotary actuated valves shall be 1% of valve travel.

The number of moving parts external to the valve and actuator shall be minimized. Exposed linkages shall be avoided where possible.

Actuation mounting shall consider service. Adequate provision shall be made for operator safety and environmental protection.

Where linear actuation is utilized the actuator design should be double acting.

Where modulating service is specified, actuators are to be fitted with positioners.

Actuators shall be sized to ensure proper valve operation at shut-off and flowing conditions. In the case of "fail open/close" operation the actuator shall operate the valve to the desired position against worst case conditions.

Electric and rotary actuators shall provide suitable means to "torque seat" to maintain Class V shut-off capabilities.



Mokveld Choke valve analysis of problems Design considerations to avoid these problems

Corrosion

Corrosion is generally associated with the choice of wrong materials. A common mistake is to use a choke valve specification based on history. It must be remembered that an oil/gas well has a process component make up that is associated with a particular well. One well may produce Carbon Dioxide, while the other doesn't. A standard specification may cause the wrong material to be selected for an application. Corrosion is relatively easily solved, as a choice of suitable materials is widely available. However a comprehensive knowledge of materials is required as combinations of certain materials may lead to galling.

Erosion

It is important to understand the difference between single and two phase scenarios.

Velocity can cause body erosion, trim erosion and piping erosion. There are different philosophies with respect to what velocities are and not acceptable, however generally selected velocities are too high. For liquid application, a rule of thumb is that the velocity has to be controlled below 5-7 m/s measured in the outlet of the flange, for two phase this is 10-15 m/s and for gas 25 - 40 m/s. It should be noted that these figures do not include for sand production and also do not take the gas/liquid ratio into account for two phase situations. It should also be noted that often choke valves are reduced in size, for example a 4 inch nominal body with 6 inch inlet and/or outlet flanges. If the velocity at the outlet flange is still within the above mentioned rule of thumb it does not automatically indicate that everything will be expected to work out, as the velocity in the so called nominal body goes up and may well exceed what is considered to be acceptable. The choke velocity should be calculated first of all with the same body and flange size before reducing the nom body size. If the velocity is lower than mentioned in the above rule of thumb, one can calculate a smaller nominal body with smaller flange. If still within the given limits a smaller body with larger flanges can be used with reduced risk of erosion.

Thus velocity is the most important design criteria, correct design limitation of this in combination with a well-designed trim will limit any erosion.

Calculating velocities has to be based on general calculations for gas, liquids and a combination of the two (two phase). A calculation is required to determine the required Cv and this can be achieved by fitting different trims in nominal body sizes. However different pipe diameter selection produces different velocities. Relatively low velocities are not advised, as the result is likely to result in the selection of a too large size choke. High velocities are likely to result in erosion of the body with an associated high maintenance cost. Trim selection is also very important. As an example Mokveld chokes are equipped with a cage provided with holes uniformly distributed over the full circumference. This design ensures that the fluid is symmetrically distributed. The many flow jets are diametrically opposed. Consequently, the energy is dissipated in the centre of the valve. This occurs in the fluid itself and not near the surface of any choke component. Also, preferential flow, the major cause of body erosion, is fully avoided.

Cavitation

Cavitation should not be taken lightly as it can not only lead to erosion but it can also cause vibration. The vibration may shatter brittle materials as Tungsten Carbide often used for the trim.

Leaking

Leaks on Choke Valves are sometimes caused by the selection of incorrect materials, but may be also attributed to general design of the Choke Valve. Some chokes have a split body design, these vary from a forged block (main body) with weld on or fitted flange connections (adapters) to main body bolted bonnet type. A one piece body casting is one answer to these problems. Also the Choke Valve seals have to fail before leaks occur. Seals utilised on almost all designs are of the 'O'Ring' type. As a choke is used under high pressure and pressure drop these O'Rings may be subjected to explosive decompression. This can cause them to split or deform. Should this happen the sealing property is lost. Explosive decompression often occurs when Viton is used. This happens to be one of the most suitable resilient materials for hydrocarbon service. Hence careful consideration of seal materials is required if Viton is selected as it is subject to explosive decompression. Furthermore the service of the O'Rings has to be considered as this can differ from static to dynamic applications. Most problems with O'Rings occur in dynamic applications.



N- line Chokes

- N-Line Valves provides engineered flow control solutions for upstream oil and gas production.
- Control Chokes and Valves are available in a full range of materials and configurations size 2" to 16" and pressure classes ASME 600 to 2500, API 2,000 to 20,000.



N-Line Plug and Cage Trim

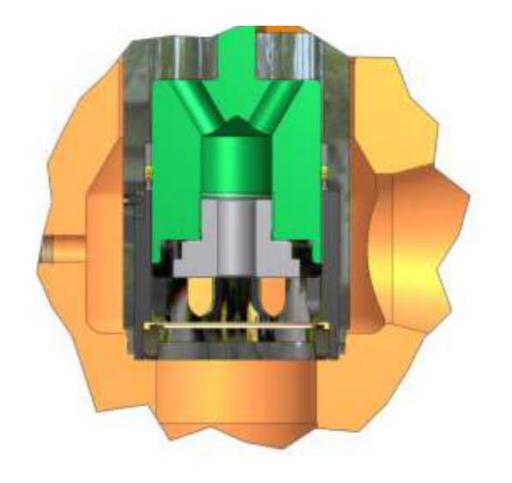
 The Plug and Cage trim type is proven for its effectiveness in high flow liquid and multi phase flow. In the closed position, the plug makes contact with a prepared shoulder in the cage to facilitate positive shut off. For Class V and VI an additional non elastomeric seal is used in the low flow area of the seat for repetitive positive shut off. This trim is available with Linear Characteristic or Equal Percent in surface hardened Stainless Steel or Solid Tungsten Carbide for erosive service. An optional full carbide plug can be used for extreme solids production.





N line High Flow Plug and Cage Trim

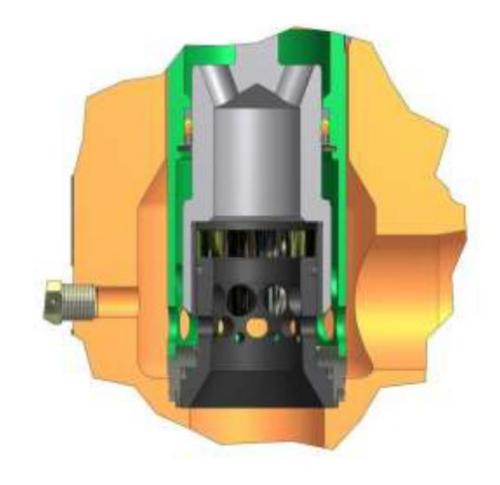
 This version of Plug and Cage trim design gives the maximum flow capacity for a cage trim choke valve. This is especially useful in low pressure drop applications and end of life wells.





N Line External Sleeve Trim

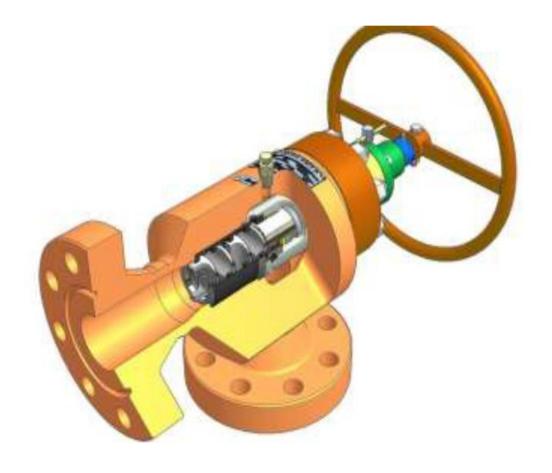
 The External Sleeve type trim uses a flow sleeve moving over the outside of a ported cage to control flow. A metal to metal seat design on the outside of the flow sleeve, out of the high velocity flow areas assures positive shut off and an extended seat life. High erosion resistance of this trim design leads to its use in severe service that may include high pressure drops and fluids with entrained solids such as formation sands. This trim is furnished in a proprietary blend of Solid Tungsten Carbide with an Equal Percentage characteristic





N-Trim Single Path-Multi Stage Trim

 The N-Trim SP is a severe service trim. solution to reduce noise, prevent cavitation and with the correct material selection, resist erosion. The trim consists of a single path multi stage plug and corresponding seats with the appropriate number of stages to prevent cavitation. Several mechanisms are utilized in the design to assist with the conversion of energy without problems of incipient cavitation in liquids. The N-Trim SP is typically applied in extreme pressure drop valves in water injection applications.





N-Trim Multi Path-Multi Stage Trim

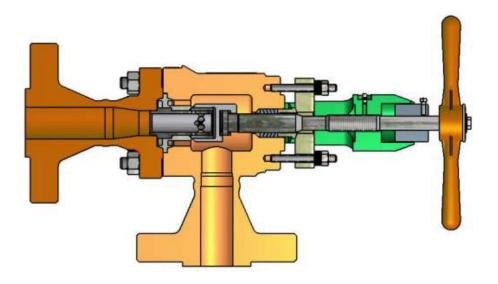
 The N-Trim MP is a severe service trim solution to reduce velocity, noise and with the correct material selection, resist erosion. The trim consists of a multi path, multi stage cage with the appropriate number of stages to remove the energy through a tortuous path. Several mechanisms are utilized in the design to assist with the conversion of energy during the pressure step down process. The N-Trim MP is typically applied in extreme pressure drop valves for gas applications





Type HTS Sleeve and Cage

 The High Temperature Closed Cage and Sleeve Assembly uses a metal to metal design to assure shut off. In the full closed position, the sleeve makes contact with the Cage Assembly in an area of low velocity making extended life of the positive seal an inherent design feature. The positive seal is bi-directional by design and will allow for reverse flow in "huff and puff" applications allowing steam injection and production in the same choke. This design is for the most severe service that may entail very high pressure drops, cavitation and entrained solids such as formation sands. This trim is available in different materials with Equal Percentage or Linear Characteristic and is available with all forms of actuators. 2" through 6" body sizes and all pressure class and size end connections are availab



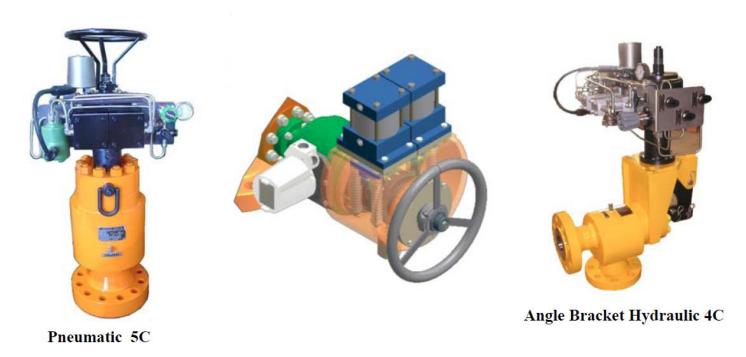


N –Line actuator

 The N-Line Valves SA-II Stepping Actuator is a pneumatically or hydraulically powered rotary indexing output actuator. The actuator consists of two power cylinder and pawl assemblies, from which the drive wheel and output shaft are driven. One operating cycle consists first of pressurizing one cylinder thereby extending the pawl to engage the drive wheel and thus incrementally rotate the output shaft in the appropriate direction, the cylinder is then depressurized retracting the pawl to its rest position. This single operating cycle rotates the output shaft of the actuator and correspondingly the valve stem by 30°. This operating cycle is repeated until the valve reaches the desired position. To drive the actuator and the valve in the opposite direction, an operating cycle is repeated using the other cylinder. When the cylinders are depressurized, the pawls are disengaged from the drive wheel, allowing the drive wheel to be rotated manually through the manual override on the outside of the actuator to position the valve. A spring detent prevents position drift from vibration. Local visual position indication is via a stainless steel micrometer for unequaled accuracy and reliability. A housing containing limit switches, a position transmitter and terminal strip is mounted externally on the yoke for direct valve stem position feedback via 4-20mA signal including HART or digital protocols. All recognized standards for electrical apparatus are available.



N line pneumatic and hydraulic actuators



SA-II Surface Stepping Actuator



Pentair choke valve Model CHV-Angle (Vonk)

- Providing superior performance in abrasive environments, precise flow control and ease of maintenance, delivering operational reliability in the most challenging applications.
- Extended service life, delivered by a robust but simple rotating disc and bean design.
- Low life cycle costs resulting from improved resistance to erosive production fluids.
- Ease of maintenance and inspection, facilitated by removal of limited internals while valve remains in service.
- Operational confidence and safety, guaranteed by 100% shut-off to Class V ANSI FCI-70.
- Operational reliability with the capability of handling high pressure drops and delivering fixed Cv values.
- Controlled environmental impact governed by reduced effects of noise and vibration.
- Improved pressure recovery performance factor delivered by the unique bean and disk design.
- Vonk chokes comply with the most stringent requirements of the European Directives and harmonized standards including Pressure Equipment Directive (97/23/EC PED) and ATEX 94/9/EC for potentially explosive atmosphere



Pentair Choke valve options

MODEL	BRAND	PRESSURE	TEMPERATURE	SIZE
Model CHV (Angle body)	Vonk	Up to Class 4500	-100°C - +300°C	DN 25-200
Model ICV (In-line type body)	Vonk	Up to Class 2500	-100°C - +300°C	DN 25-50
Model SCV (Angle body)	Vonk	Up to Class 2500	-46°C - +250°C	DN 25-80
Model YCV (Y-type body)	Vonk	Up to Class 4500	-100°C - +300°C	DN 25-200



Samson / Ringo Valvulas SL Profile

- choke valves have been developed to cope with high pressure drop applications on liquid, gas or multiphase fluids for oil
 and gas wells; used in production, gaslift-topside and water injection applications. Special designs include low noise or
 anti-cavitation features. Materials are selected to withstand erosion. Interchangeable beans allow the use of the same
 valve at different conditions.
- applications include refineries, chemical and petrochemical industry, oil and gas upstream, midstream and downstream,
 offshore, water treatment and energy generation plants (nuclear, fossil, combined cycle and thermosolar).
- ISO 9001-2008 by Lloyds register, CE stamp also by Lloyd's Register, TÜV, API 6D, API 6A, API 6DSS and ASME III N and NPT stampsenvironmental protection and health and safety responsibilities being certified according to ISO 14001 and OHSAS 18001.



Subsea Chokes International (SCI)

- Retrievable Subsea Chokes
- Fully Operational in the Most Challenging of Deepwater, High Pressure Offshore Environments
- Significantly greater resistance to erosion than current choke solutions.
- Operational with pressures at the wellhead of up to 20,000 PSI
- Flexibility regarding sizing Cvs from 100 to over 1000
- A new simplified actuation technology.
- Real-time information during production

Product Specs General specifications:

- Pressure rating: 20,000 PSI / 1,380 Bar
- Temperature rating: -60F 350F / -50C 180C
- CV range: 40 1000
- Line size: 4" 10"
- Complies to all relevant ISO and IPO standards
- Standard ROV interfaces
- Fully redundant instrumentation
- Pressure / temperature
- Erosion measurements of critical areas
- General condition monitoring
- Positional indication with high accuracy

